

PIPENET® NEWS

AUTUMN 2019

LEADING THE WAY IN FLUID FLOW ANALYSIS



PIPENET VISION[®] 1.10.0 RELEASE

Welcome to PIPENET VISION 1.10.0!

We are pleased to deliver some fabulous enhancements across all modules to save time and make the PIPENET experience even better.

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PIPENET Vision 1.10.0 will soon be sent to all customers with active PIPENET Maintenance, Updates and Support and/or active 5-year and 1-year licences. Please contact us if you do not receive it by the middle of December. If you are not a current customer and you would like a copy of PIPENET VISION 1.10.0, please contact us at pipenet@sunrise-sys.com

PIPENET Training Materials

Did you know that you can easily master PIPENET by following the examples in our excellent Training Manuals? Training Manuals for all modules are inbuilt in PIPENET. They provide detailed step-bystep guidance and have plenty of practical examples. Data files for all examples are also provided. You can find all the training materials at: **PIPENET > Help > Learning > Training Materials**

PIPENET at OTC and Gastech: thank you to everyone who visited us in Houston

PIPENET was a great success again at leading trade shows in Houston this year. We were happy to meet our customers and all other visitors at OTC-2019 in May and at Gastech-2019 in September. Our booth visitors had a great opportunity to see a live demonstration of PIPENET, ask questions and receive answers. Thank you to everyone who visited our booths. We will be happy to meet you again next year!

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PIPENET VISION[®] 1.10.0 Release

Welcome to PIPENET VISION 1.10.0!

We are pleased to deliver some fabulous enhancements across all modules to save time and make the PIPENET experience even better.

PIPENET Vision 1.10.0 Transient Module

- Dry Pipe 2 including calculation of air pressure
- New air valve component
- The Scenario Manager facilitates easy comparison of a range of scenarios on one screen.
- Improved searching in Forces dialog.
- Improvements to the graph viewer.
- RES2CSV utility now includes option to export to Excel.

PIPENET Vision 1.10.0 Spray/Sprinkler Module

- Improved formatting of the NFPA report.
- Updated Chinese Standard.

PIPENET Vision 1.10.0 Standard Module

• Non-Newtonian power-law fluids can now be modelled in the Standard Module.

PIPENET All Modules

- Measure and calculate using 'litres per second'.
- Improved output formatting.
- Module name displayed in title bar.

Dry Pipe 2 model – outstanding capability of PIPENET Transient Module for modelling air volume in pipes

One of the powerful, new developments introduced in **PIPENET Vision 1.10.0** is the 'Dry Pipe 2' Model in PIPENET Transient Module.

Dry Pipe 2 Model allows air to flow into the system and considers the effect of air volume in pipes.

Dry Pipe 2 Model can simulate complex pipe networks, including:

- dry pipes
- wet pipes and
- components other than pipes.

Q: What is the purpose of the Dry Pipe Model?

- 1. Improve modelling accuracy by considering the effect of air volume in pipes.
- 2. Estimate the priming time of dry deluge systems.
- 3. Evaluate the pressure surge during the priming of a dry system.

Q: What are the differences between Dry Pipe 1 Model and Dry Pipe 2 Model?

- 1. Dry Pipe 1 Model assumes air pressure is constant 0 barg while Dry Pipe 2 Model calculates air pressure based on the ideal gas law PV = nRT under isothermal conditions.
- 2. Dry Pipe 2 Model considers the friction loss of air flow in components (e.g. valve, nozzle etc.) while Dry Pipe 1 Model ignores it.
- 3. Dry Pipe 1 Model is usually faster than Dry Pipe 2 Model. Both the models can give accurate results if air pressure is around 0 barg. Otherwise, Dry Pipe 2 Model provides a better accuracy.

Q: What are the differences between the Caisson Models and Dry Pipe 2 Model?

The caisson Models are composed of three components:

- a dry or partially filled pipe,
- a non-return valve and
- an air valve,

and their location is fixed, see the figure below on the left.

Dry Pipe 2 model is more flexible, which allows to build a more complex dry network, see the figure below on the right.





- 1. The non-return value in the Caisson Model continues at a closed state, before the caisson is primed, so that the air value is the only path for the air flow. There is greater flexibility in the Dry Pipe 2 Model.
- 2. The Two-Node Caisson Model can consider wave propagation at all states. The Dry Pipe Model assumes the wave passes through it instantly.
- **Q**: What are the differences between the Vacuum Breaker Model and the Air Valve Model?
- 1. The Vacuum Breaker Model and the Air Valve Model can give same/similar results if the air volume is not large enough to affect the local flow conditions. In this case, the Vacuum Breaker Model is recommended because it is simpler and usually faster.
- 2. The Vacuum Breaker Model stores the inflow air so that the nearby pipes keep at wet state. The Air Valve Model allows the inflow air to flow into the nearby pipes and also can release the air in the nearby dry pipes.

Q: How to activate the Dry Pipe Model?

In "Network Options" window, Dry Pipe 1 Model can be activated by unticking the option of "Treat all pipes as wet" and unticking the option of "Consider air-cushion effect".

Dry Pipe 2 Model can be activated by unticking the option: "Treat all pipes as wet" and ticking the option "Consider air-cushion effect".

| twork | k Options | | | | | | | | ſ | > |
|-------|----------------------------------|------------|---------|------------|------------|---------|---------------------------|-------|---|---|
| tle | Module Options | Units | Fluid | API Fluid | Pipe types | Display | Network templates | | | |
| | Simulation time | s | | | | | Defaults | | | |
| | Simulation star | ts (sec) | | 0 | | | Roughness (mm) | Unset | | |
| | Simulation stop | os (sec) | | 100 | | | Elevation (m) | 0 | | |
| | User Define | ed Timest | ер | Variable T | ìmestep | | K-factor | 0 | | |
| | Calculation tim | estep (se | ec) | 0.005 | | | Diameter (mm) | Unset | | |
| | Ambient condi | tions | | | | | Wavespeed | | | |
| | Ambient pressu | ire (Pa A |) | 101325 | | | Default wavespeed (m/sec) | 1260 | | |
| | Ambient tempe | rature (90 | C) | 15 | | | User Defined Pipe Waves | peeds | | |
| | Force options | | | | | | Cavitation | | | |
| | Output tota | l forces | | | | | O No cavitation | | | |
| | Output dyn | amic for | es | | | | Vapour cavitation only | | | |
| | Time to start D Results (sec) | lynamic F | orce | Unset | | | Channel cavitation only | | | |
| | Pressure Drop | Model | | | | | Dry Pine | | | |
| | Coulson and | d Richar | dson | | | | Treat all pipes as wet | | | |
| | O Colebrook- | White | | | | | Consider air-cushion effe | ct | | |
| | | | | | | | New pipes wet | _ | | |
| | Hydraulic grad | ient calc | ulation | | | | ○ New pipes dry | | | |
| | Reference nod | e label | | 2 | | | | | | |
| | Reference nod | e elevati | on (m) | -20 | | | | | | |
| | | | | | | | | | | |
| | | | | | | | | | _ | |

Q: What are the typical applications of the Dry Pipe 2 Model?

1. Dry Pipe 2 Model can simulate complex dry networks. For example, the PIPENET Model on the right below can simulate the firewater system on the left accurately. The dead end is modelled by a zero-flow specification.



2. Dry Pipe 2 Model can improve calculation accuracy and simplify simulation Model. The model below is a typical example to calculate the priming time and pressure surge in a dry deluge system.



3. Dry Pipe 2 Model allows air to flow into the system and considers the effect of air volume on the system static head. In the cooling water system below, the Dry Pipe Model can predict the pump trip/reverse speed accurately.



6

Q: What are the limitations of the Dry Pipe Model?

- 1. The friction loss of air flow is negligible in the pipe model.
- 2. One pipe only has one air bubble/slug. If both the inlet and outlet of a pipe are dry, the whole pipe is at dry state.
- 3. Dry state cannot coexist with channel cavitation state in a single pipe.
- 4. In Dry Pipe 1 Model, it is assumed that the air pressure is constant 0 barg, i.e. the pressure loss of air flow is ignored. In addition, there is no obstacle to block air flow to atmospheric exit. Items such as wet pipe, short pipe, caisson, simple tank, accumulator and closed valves can create a restriction and increase the pressure above 0 barg.
- 5. In Dry Pipe 2 Model, the air pressure need not be 0 barg as long as air properties can be calculated based on the ideal gas law, under isothermal conditions. The pressure loss in components considers both subsonic and sonic states. In addition, air flow will convert to the same volume liquid flow in the following cases: (a) the air-liquid mixture is not stratified flow; (b) air flow into short pipe, pipe bundle, caissons, simple tank and accumulator.

Scenario Manager: Purposes and User Guide

Purpose of the Scenario Manager

The scenario manager is intended to make it easy to create variations on a network design and compare the relative performance of those variants. This can be useful for optimising networks, for example.

Without the scenario manager, the user themselves must

- Make multiple copies of the network.
- Modify each copy, by hand, to reflect the changes that they want to try.
- Run PIPENET® Vision on each modified file in turn to generate the results.
- Compare the results. For example, for a transient network the user would need to open the graph viewer and open each .res file.

The scenario manager allows the user to do these steps much more easily.

In the first version of the scenario manager, the user will be limited to modifying Specifications. However, subsequent versions will support further modifications.

Preparation for Use

The overall process for using the scenario manager to create a new scenario-set is as follows:

1. Create the master model (the network on which the scenarios will be based).



2. Identify the Specification(s) that will be changed in the scenario (via the node to which they apply).

| etrochemic | al plant 100 m | | |
|------------|------------------------------|--------|-------|
| ⊜-C | Insert Node | | eline |
| | Explode Node | | |
| | Delete | | |
| | Reverse | | |
| | Delete Waypoints | | |
| | Сору | Ctrl+C | |
| | Paste | Ctrl+V | |
| | Paste (incl. layout) | | |
| | Cut | Ctrl+X | |
| | Include Spec. in scenarios | | |
| | Exclude Spec. from scenarios | | |
| < | Select Results | | |

3. Start the scenario manager.

| Tools Window Help | | |
|------------------------|---|------------------------------|
| Tag selected items | > | |
| Remove tags | > | - U |
| Make path | | Tools 🔓 🕀 [|
| Export clipboard | | |
| Export HP-GL/2 | | |
| Export DXF file | | |
| Reverse selected pipes | | Co |
| Add mutiple pipes | | Ani |
| Utilities | > | PIPENET XML to Excel |
| | | PIPENET RES file to CSV |
| | | Convert a Model to Transient |
| | | Scenario Manager |
| | | |

4. Select the master model to use as the basis for the new scenario-set.

| | New Scenario Set | X | |
|----------------------|-------------------|--------------------------------|---|
| Master model | | D:\dave\work\LoadingSystem.sdf | |
| Scenario set name | LGEN project 7A48 | | |
| Scenario set descrip | tion:- | | |
| 500N Transfer line | | | |
| | Ok | Cancel | 1 |

5. The scenario manager presents the master model as a read-only scenario (for comparison).



6. Click the blue "Add scenario" button and modify the scenario name and specification(s) in the new scenario as required.



7. Repeat 6. until all of the scenarios that are needed have been defined.



8. Save the scenario set, to remember the scenarios defined and the values changed.

| | New Open Save Save as Close Exit | Load | led Scenario Se | t name: LGEN projec | :t 74 |
|--|--|---------------------|-----------------|---------------------|---------------|
| Save Scenario | Set as | | | | × |
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| Organise 🔻 | New folder | | ~ | | EE 🔹 😮 |
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| | · · · · · · · · · · · · · · · · · · · | < | | | > |
| File nar | ne: LoadingSystem. | sns | | | ~ |
| Save as ty | pe: PIPENET Scenari | o Set files (*.sns) | | | ~ |
| ∧ Hide Folders | | | | Save | Cancel |

9. Click the Generate button on the ribbon. As the help says, this will make a copy of your master model for each scenario and automatically edit the copy to apply the specification changes that you have set.



10. Click the run button to automatically run PIPENET® Vision on each of the scenario models.



11. Click the View results button to compare the results of the scenarios.

| | | | | Loaded | Scenario Set | name: LGEN |
|---|----------|---------------|----------------------------|---|----------------------------|------------|
| | File | Home | Setu | р | | |
| | 0 | | | 2 | | |
| | Generate | e Run Cancel | View | Edit Name and | d View | Expor |
| | | | results | Description | changes | scenario n |
| | | Control | | Edit | View | |
| | Action | Scenario name | Viev | w the last run's | results. | |
| 4 | | Master values | 3 | View the res last run of the set. | ults of the he scenario | |
| | | Scenario 1 | 🕜 Pre | ss F1 for help | | |
| | X | | Time f | unction: Co | nstant value | |
| | | | Consta | ant 0.8 | } | |
| v | × | Scenario 2 | Physic Time f Consta | al Quantity: Set unction: Co ant 0.6 | ting nstant value | |

| Results of running scenario set 'l | GEN project 7A48 | Х | | | | |
|------------------------------------|------------------|---|--|--|--|--|
| Manhaninakan | View output | | | | | |
| Master values | View max/min | | | | | |
| | View output | | | | | |
| Scenario 1 | View max/min | | | | | |
| | View changes | | | | | |
| | View output | | | | | |
| Scenario 2 | View max/min | | | | | |
| | View changes | | | | | |
| | View output | | | | | |
| Scenario 3 | View max/min | | | | | |
| | View changes | | | | | |
| Compare results in graph viewer | | | | | | |
| Done | | | | | | |

For a transient model, click the "Compare results in graph viewer..." button. This will start the graph viewer with the graphical result (.res) file for each scenario already loaded.



12. Now you can display the curve of interest for each of the scenarios.



13. Having chosen the scenario that best matches the requirements, use the "Export scenario model..." button to save a copy of the sdf/slf files for that scenario with the relevant specification values.



| Export Scenario Model | | _ | × |
|--------------------------|---------------------------------|------|---|
| Scenario model to export | Scenario 2 | | ~ |
| Export to folder | D:\dave\work | | |
| Exported model name | LoadingSystem-selected scenario | .sdf | |
| | Export Cancel | | |

14. If you wish to add extra specifications to the scenario or remove existing ones, use the "Edit the master model" button to start PIPENET with the master model open and ready to modify. Once you have made the changes, it is important to save the PIPENET master model.

| File Edit View Librarie | es Options Colouration | Calculation | Output | Tools Wi | indow H | lelp | | | | | |
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15. Return to the scenario manager. If the scenario set is still open, close it and then open it again to pick up the master model changes.



16. The Scenario Manager will recognise that changes have been made and tell you what has changed. It will attempt to keep as much of your original scenario changes as it can and show the additional specifications.

| | Opened Scenario Set updates. | × |
|---|--|---|
| 0 | Master-model has changed and the following changes have been made to th opened Scenario Set These nodes have been added and their specifications included:- 7 | e |
| | OK | |

| | | Load | ded Scenario Set r | name: LGEN project | 7A48* | | |
|----------|---------------|--|---|--|---------------------------------------|----------------|--|
| File | Home | Setup | | | | | |
| Generate | Run Cancel | View results | e and View changes View | Export scenario model Mod | Edit the master model els | Exit System | |
| Action | Scenario name | i/1 | | 7 | | | |
| | Master values | Physical Quantity: Time function: Constant | Setting Constant value 1 | Physical Quantity: Time function: Constant | Pressure Constant value 0 bar G | | |
| × | Scenario 1 | Physical Quantity: Time function: Constant | Setting Constant value <mark>0.8</mark> | Physical Quantity: Time function: Constant | Pressure Constant value 0 bar G | | |
| × | Scenario 2 | Physical Quantity: Time function: Constant | Setting Constant value <mark>0.6</mark> | Physical Quantity: Time function: Constant | Pressure Constant value 0 bar G | | |
| × | Scenario 3 | Physical Quantity: Time function: Constant | Setting Constant value 0.4 | Physical Quantity: Time function: Constant | Pressure Constant value 0 bar G | | |
| + | Add scenario | | | | | | |

17. Do not forget to save the changes that you have made, or use "Save as" if you would like to retain both the original and new version of the scenario set scenario-set.

| | ٠ | | Loaded Scen | ario Set name: LGEN p | vroj |
|--|-------------------|-------------|-------------------|-----------------------|------------------|
| | New | | | | |
| | Open | | | | |
| | Save | | | | |
| | Save as | | | | |
| | Close | | | | |
| | Exit | | | | |
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| | | | | | |
| Save Scenario Set a | as | | | | × |
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| ∧ Hide Folders | | | | Save | Cancel |

18. When you Save-As you are encouraged to update the scenario set name and description.



19. You can do that via the "Edit Name and Description" button.

| | | | Load | ded S | cenario Set i | name: LG | EN project | 7A48 |
|----------|--------------------------------|--------------------------------------|-----------------------|-----------------------|---|---------------------------|----------------------------|-----------------------|
| File | Home | Setup |) | | | | | |
| Generate | Run Cancel | View results | Edit Name Descript | and ion | View changes | Ex scenar | port io model | Edit master |
| | Control | | | | View | | Mode | els |
| Action | Scenario name Master values | i/1 Physica Time fu Constar | Edit th name a | e curi and d Ed | rent Scenari escription. it the Scena | io Set rio Set. | Quantity: nction: t | Pressu Consta 0 |
| × | Scenario 1 | Physica Time fu Constar | ? Press | F1 fo | or help | Constar | Quantity: action: at | Pressu Consta 0 |
| | Scenario 2 | Dhusica | Ousetitus | C++: | ~~ | Dhusical | Ousatitu | Droccu |

| Edit Scenario Set Description | | | | | | | |
|--|---|--|--|--|--|--|--|
| Scenario set name LGEN project 7A48 inc node 7 Scenario set description:- | | | | | | | |
| 500N Transfer Line | | | | | | | |
| Ok Cancel |] | | | | | | |

New Chinese Standard (GB) in the Spray/Sprinkler Module

The latest Chinese Standard (*Code of Design for Sprinkler Systems GB 50084-2017, National Bureau of Quality and Technology Supervision, P.R. China and Ministry of Construction, P.R. China, May 27 2017*) has been introduced to the Spray/Sprinkler Module. The new standard can be selected from the Menu | Options | Module options. The previous Chinese Standard has been kept to allow users to run their old models.

| Netwo | ork Options | | | ? | × | |
|-------|--|-----------------------|--|--|---|--|
| Title | Module Options (| Units Pipe types | Display Calculation Tables Network templates | Defaults | | |
| | Intel Module Options Onits Pipe types Display Design Rules ONFPA pre-1996 ONFPA 2013 Onwards O O NFPA 2013 Onwards O E OLDFOC OLDFOC O Chinese Standard (GB) pre-2017 Image: Chinese Standard (GB) 2017 Onwards Elevations Use pipe/duct elevations O Use node elevations Vamings Control O Treat warnings as errors | | Pressure Drop Model Darcy Hazen-Williams Chinese Standard (GB) pre-2017 Orifice Plate Model BS. 1042 Heriot-Watt Crane Chinese Standard (GB) Fluid Water at 20°C User Defined Density 998.2343 Viscosity 0.001 | Velocity Pressure Options Velocity Pressure Model ONFPA Fomula Standard formula Ignore Pressure Loss at Entrance Ignore Include Pressure Loss at Exit Ignore Include | | |
| | Spi | ray or Sprinkler mode | e construction of the second s | zzles off) OK Cancel Apply | | |

Non-Newtonian Power-Law Fluids in the Standard Module

The power-law fluid is a type of non-Newtonian fluid characterized by a flow behaviour index and flow consistency index. This can now be modelled in the Standard Module. The new fluid can be chosen through: Menu | Options | Fluid.

| Module Options | Units | Fluid | Heat Transfer | Pipe types | Display | Calculation | Tables | Network temp | lates | Defaults |
|---|--|-------|---------------|------------|---------|--|--|--------------|--------------------|----------|
| Fluid Class | | | | | | | | | | |
| water liquid, property cor liquid, direct speci liquid, variable pro steam Van der Waals ga ideal gas low pressure gas medium pressure g Advanced fluid Power law | rrelations fication perties is gas | | | | | Properties Density (kg Behaviour Consistend | g/m ³) index, n cy index (| (Pasri) | 960 0.3 1.48 | |
| Gas oxygen nitrogen carbon dioxide air water vapour methane propane user defined | | | | | | | | | | |
| | | | | | | Fluids Librar | у | | ~ | |
| | | | | | | | | S | ave as | defaults |
| | | | | | | | | | | |

New 'Litres per Second' Unit in All Modules

A new flowrate unit, litres per second, has been added to all modules. The new unit can be chosen from Menu |Options |Units.

| Network Options | | ? × |
|---|--|---|
| Network Options Title Module Options Units Pipe types Display Calculation System SI System SI Metric British US User defined Length Diameter Velocity Temperature Density Viscosity Pressure Flow type Volumetric flow m ² /s Mt ² /s ft ³ /min US gal/min US gal/min | Tables Network templates Defaults Display precisions - Volumetric flow G General use Schematic Drawings Conversion tool - Volumetric flow Image: Conversion tool - Volumetric flow Image: Image: Conversion tool - Volumetric flow Image: Conversion tool - Volumetric flow Image: Image: Image: Conversion tool - Volumetric flow Image: Conversion tool - Volumetric flow Image: Image | ? × 0.1 `` 0.1 `` 0.1 `` 0 `` 0 `` 0 `` 0 `` 0 `` 0 `` 0 `` 0 `` 0 `` 0 UK gal/min 0 US gal/min 0 brls/day 1it/min `` 1it/s `` |
| | | Save as defaults for new files |
| | | |
| | ОК | Cancel Apply |